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Supporting Information

Designed Precursor for the Controlled Synthesis of Highly Active Atomic and Sub-nanometric Platinum Catalysts on Mesoporous Silica

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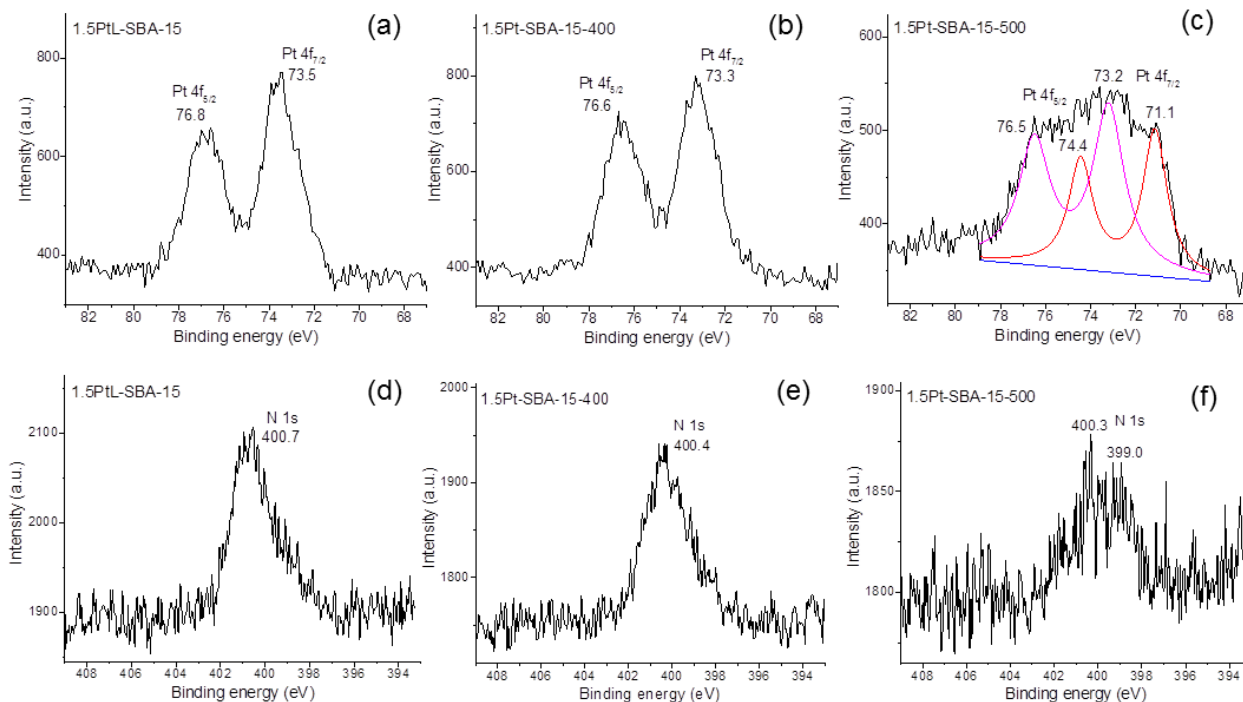


Fig. S1 XPS spectra of SBA-15 supported Pt-complex (1.5 wt% Pt loading) at different temperature: (a, d) before the heat treatment, (b, e) 400 °C, (c, f) 500 °C.

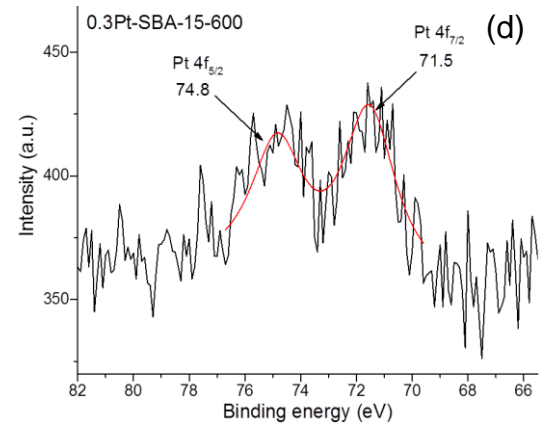
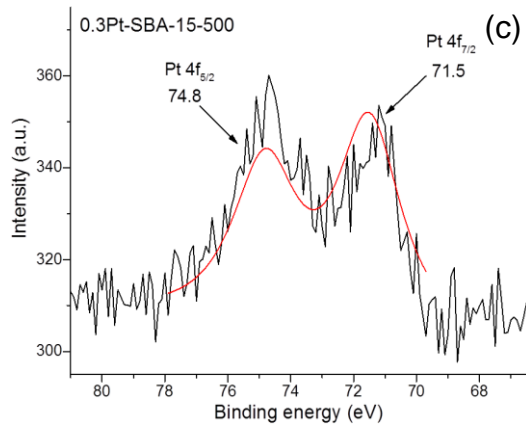
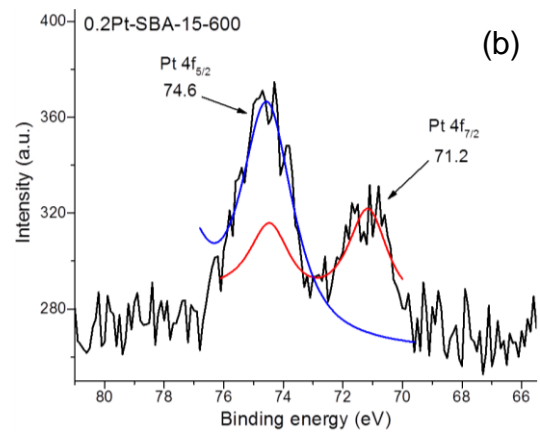
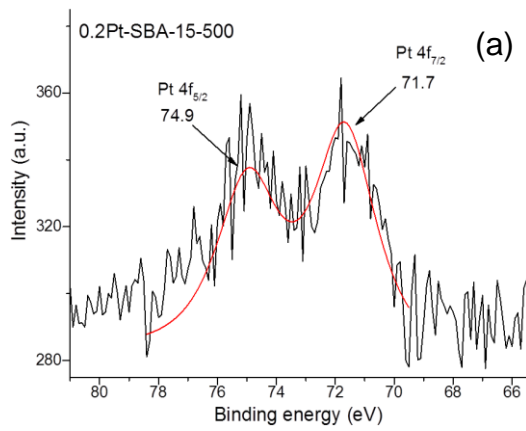
Table S1 Elemental analysis results of samples treated at different temperature.

Sample	C (%)	H (%)	N (%)
SBA-15	ND	1.3	-
1.5PtL-SBA-15	2.49	1.74	0.65
1.5Pt-SBA-15-400	1.67	1.43	0.71
1.5Pt-SBA-15-500	<0.50	1.25	0.52

ND: not detected due to very low carbon content.

Table S2 Nitrogen content in different samples treated at different temperature measured by XPS.

Sample	1.5PtL-SBA-15	1.5Pt-SBA-15-400	1.5Pt-SBA-15-500
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(e)

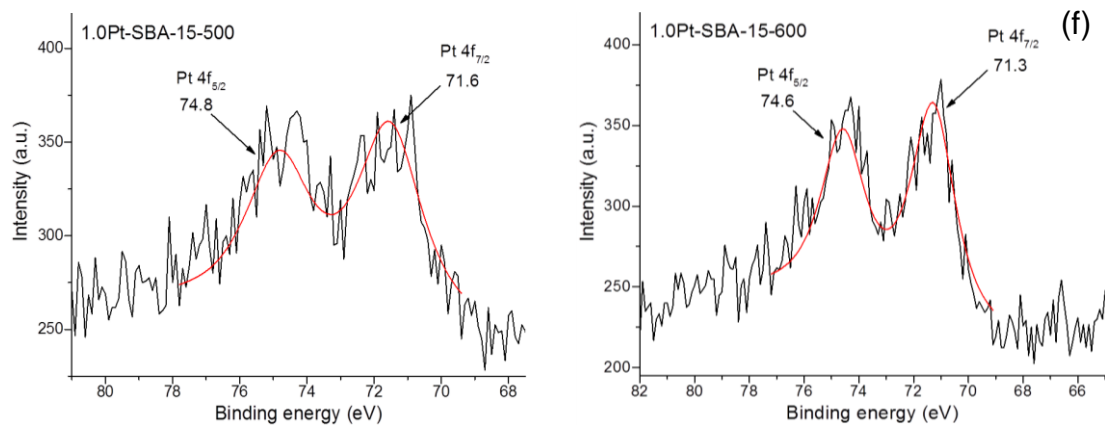


Fig. S2 XPS spectra of (a) 0.2Pt-SBA-15-500, (b) 0.2Pt-SBA-15-600, (c) 0.3Pt-SBA-15-500, (d) 0.3Pt-SBA-15-600, (e) 1.0Pt-SBA-15-500, (f) 1.0Pt-SBA-15-600.

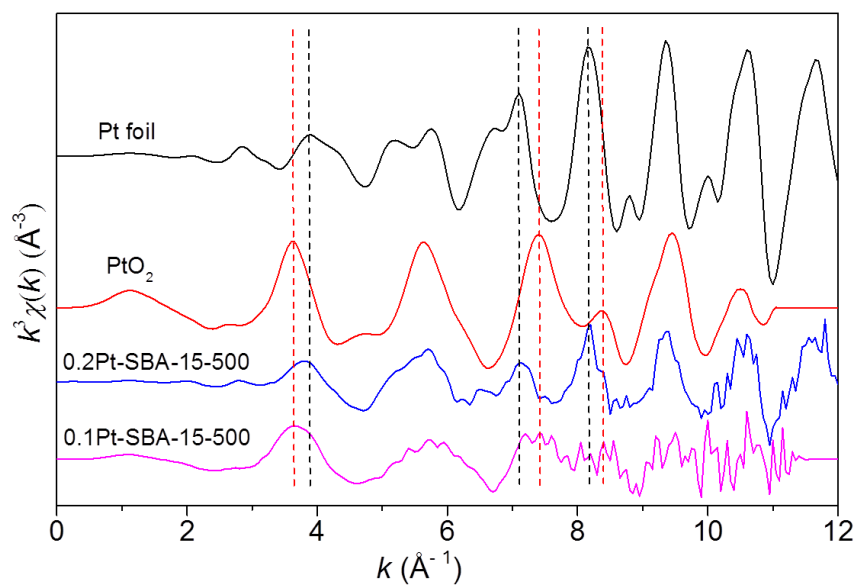
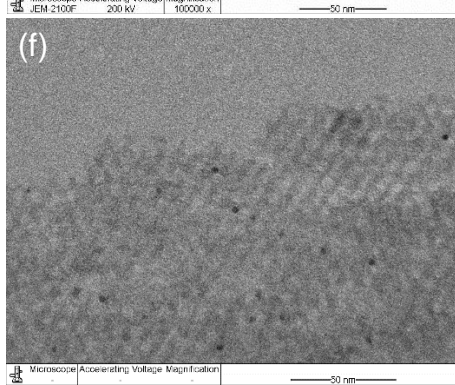
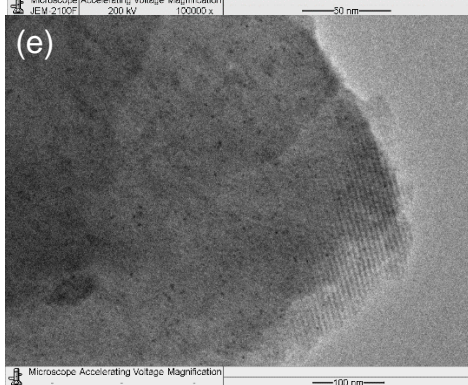
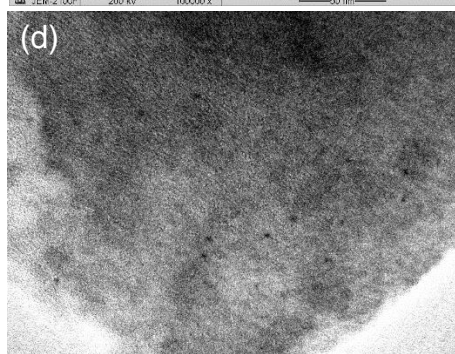
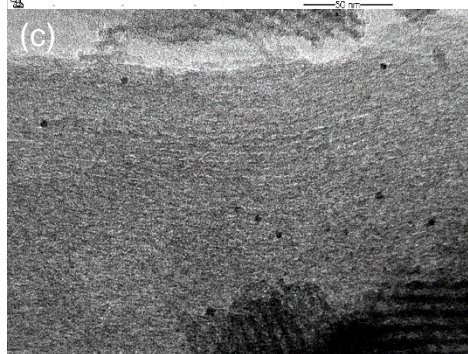
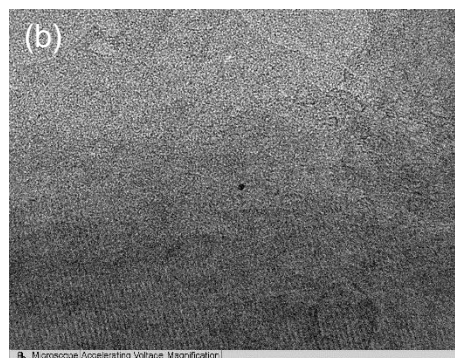
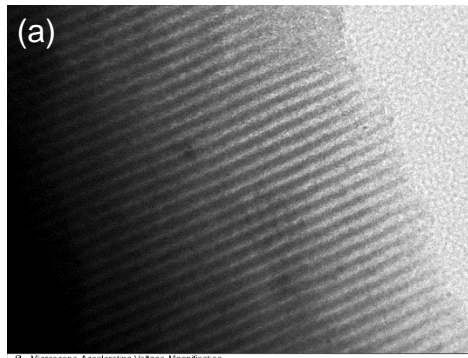


Fig. S3 k^3 -weighted k -space spectra at the Pt L₃-edge for different Pt samples. Black dashed lines refer to the phase for Pt-Pt contribution and red dashed lines refer to the phase for Pt-O contribution.



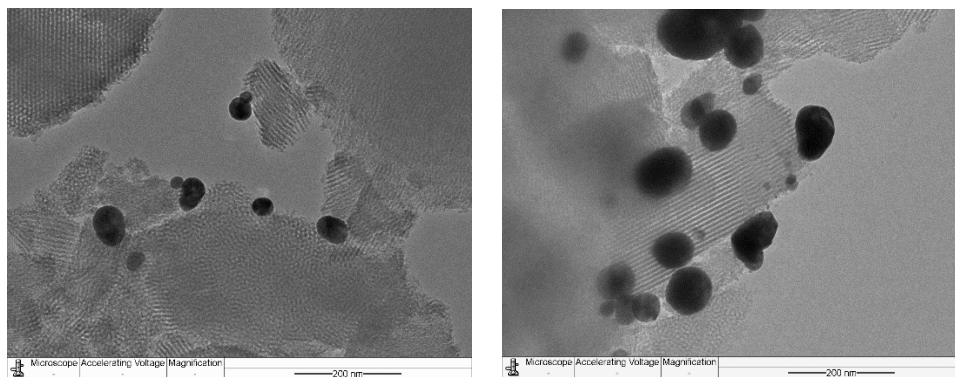


Fig. S4 TEM images of (a, b) 0.2Pt-SBA-15-600, (c, d) 0.3Pt-SBA-15-500, (e, f) 1.0Pt-SBA-15-500, (g) 0.3Pt-SBA-15-500-C, (h) 1.0Pt-SBA-15-500-C.

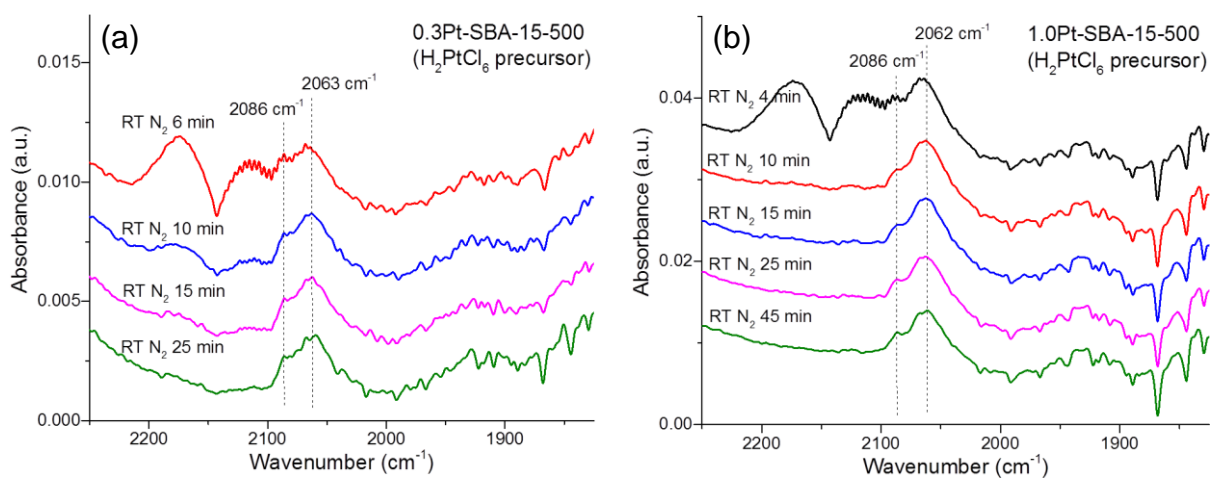
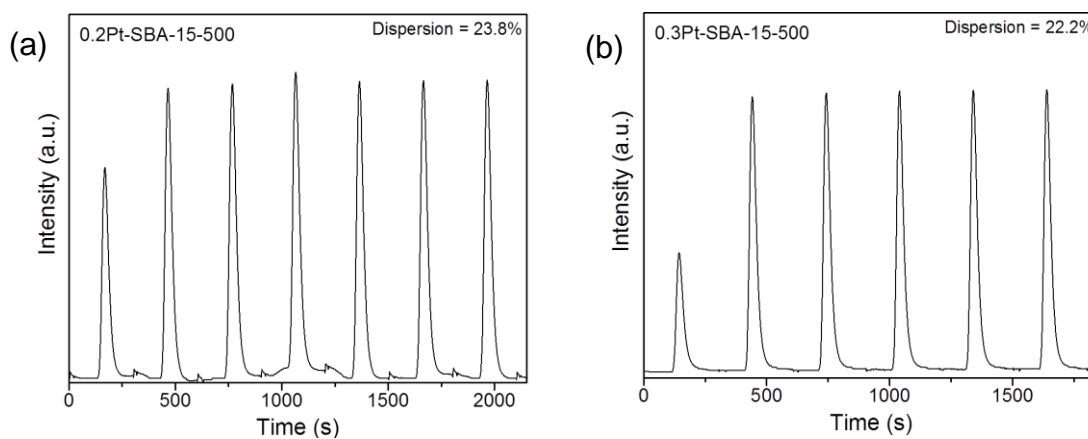


Fig. S5 IR spectra of CO adsorbed on different samples: (a) 0.3Pt-SBA-15-500-C, (b) 1.0Pt-SBA-15-500-C.



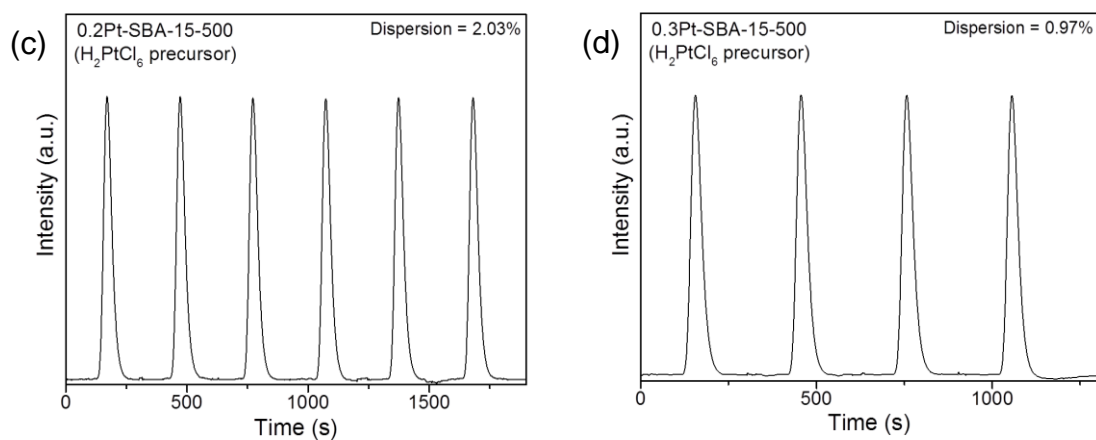


Fig. S6 H₂ pulse titration profiles of samples after treatment with air: (a) 0.2Pt-SBA-15-500, (b) 0.3Pt-SBA-15-500, (c) 0.2Pt-SBA-15-500-C, (b) 0.3Pt-SBA-15-500-C.

Table S3 Elemental analysis results of [Pt(^tBu₃tpy)Cl]Cl·H₂O complex.

Element	C	H	N
Calculated (wt%)	47.30	5.44	6.13
Found (wt%)	47.07	5.28	6.07

Table S4 Selective hydrogenation of phenylacetylene (PhAc).^a

Entry	Catalyst	PhAc/Pt	<i>t</i> (min)	Conv. (%)	S _{Styrene} (%)	S _{Ethylbenzene} (%)	Specific activity (mol _{sub} /mol _{Pt} h)
1	0.2Pt-SBA-15-500	4000	15	24.3	94.1	5.9	3888
2	0.3Pt-SBA-15-500	4000	15	30.6	92.5	7.5	4896
3	0.2Pt-SBA-15-500	4000	60	64.8	89.4	10.6	
4	0.3Pt-SBA-15-500	4000	60	87.2	86.1	13.9	
5	1.0Pt-SBA-15-500	4000	60	99.6	67.6	32.4	
6	0.3Pt-SBA-15-500-C	4000	60	28.3	89.5	10.5	1132
7	1.0Pt-SBA-15-500-C	4000	60	24.3	94.2	5.8	972
8	0.2Pt-SBA-15-500-C	1000	120	63.0	85.7	14.3	
9	0.3Pt-SBA-15-500-C	1000	120	86.3	77.9	22.1	
10	1.0Pt-SBA-15-500-C	1000	120	35.4	82.5	17.5	

^aReaction condition: phenylacetylene = 18.9 mg (0.1845 mmol), 2 mL methanol, 10 bar H₂, room temp.

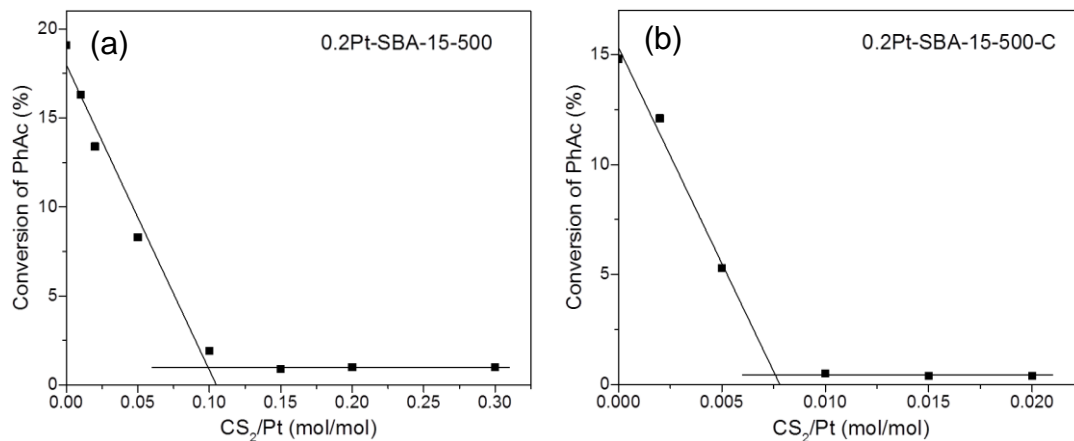
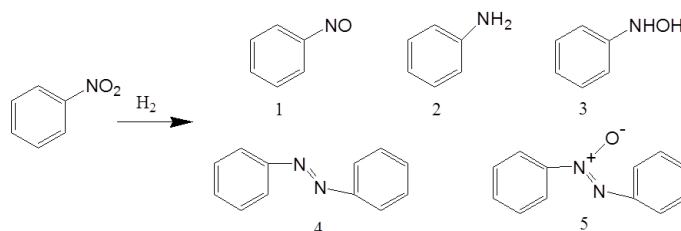


Fig. S7 Conversion of phenylacetylene over (a) 0.2Pt-SBA-15-500 and (b) 0.2Pt-SBA-15-500-C as a function of CS_2/Pt . Reaction conditions: (a) PhAc/Pt = 4000, solvent = methanol (2 mL), 10 bar H_2 , room temperature, $t = 15$ min; (b) PhAc/Pt = 1000, solvent = methanol (2 mL), 10 bar H_2 , room temperature, $t = 30$ min. In each case, 5 mg of catalyst was poisoned with certain amount of CS_2 dissolved in methanol prior to the addition of phenylacetylene.

From the fitting curves, by assuming one CS_2 molecule blocking two active sites, the active sites fractions of 0.2Pt-SBA-15-500 and 0.2Pt-SBA-15-500-C catalysts were 20% and 1.5%, respectively.

Table S5 Hydrogenation of nitrobenzene (NB).^a

Entry	Catalyst	NB/Pt	H ₂ (bar)	<i>t</i> (min)	Conv (%)	Sel 1 (%)	Sel 2 (%)	Sel 3 (%)	Sel 4 (%)	Sel 5 (%)
1	0.2Pt-SBA-15-500	4000	10	15	100	24.4	47.2	0	0	28.4
2	0.2Pt-SBA-15-500	4000	10	60	100	15.7	58.3	0	0.7	25.3
3	0.2Pt-SBA-15-450	4000	10	15	6.4	0	100	0	0	0
4	0.2Pt-SBA-15-450	2000	10	15	100	19.9	64.1	0	0	16.0
5	0.2Pt-SBA-15-500	8000	10	15	68.2	32.2	61.8	0	0	6.0
6	0.2Pt-SBA-15-500 (10 °C)	4000	10	15	16.4	0	100	0	0	0
7	0.2Pt-SBA-15-500 (60 °C)	4000	10	15	100	15.1	79.5	0	0	5.4
8	0.2Pt-SBA-15-500	4000	10	10	100	39.5	45.4	0	0	15.1
9	0.2Pt-SBA-15-500	4000	2	15	100	32.0	59.9	0	0	8.1
10	0.2Pt-SBA-15-500	4000	5	15	100	35.4	58.1	0	0	6.5
11	0.2Pt-SBA-15-500	4000	20	15	100	38.7	53.9	0	0	7.4
12	0.2Pt-SBA-15-500 (EA 50)	4000	10	15	76.1	7.7	33.9	0	0	58.4
13	0.2Pt-SBA-15-500 (EA 50)	4000	2	30	3.0	0	0	0	0	100
14	0.2Pt-SBA-15-500 (EA 50)	4000	5	30	36.5	5.6	28.7	0	0	65.7
15	0.2Pt-SBA-15-500 (EA 50)	4000	5	60	100	7.9	25.6	0	0	66.5
16	0.2Pt-SBA-15-500-C	4000	10	15	0	0	0	0	0	0
17	0.2Pt-SBA-15-500-C	4000	10	60	5.2	0	100	0	0	0
18	0.2Pt-SBA-15-500-C	2000	10	60	19.0	0	100	0	0	0

^aReaction condition: NB = 22.7 mg (0.1845 mmol), 2 mL methanol, room temp. EA: ethanolamine (50 μL).

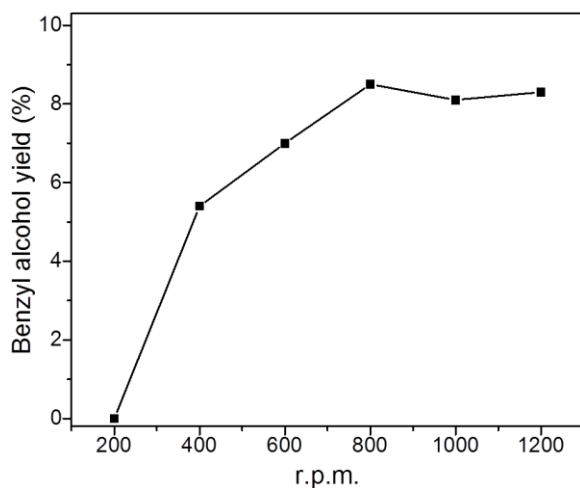


Fig. S8 Benzyl alcohol yield against rotation per minute (r.p.m.) using 0.2Pt-SBA-15-500 catalyst. Reaction conditions: catalyst = 12 mg, benzaldehyde = 6.2 μ L, benzaldehyde/Pt = 500, solvent = methanol (2 mL), H_2 pressure = 10 bar, room temperature, t = 30 min.

Table S6 Hydrogenation of benzaldehyde (BZ).

Entry	Catalyst	BZ/Pt	T ($^{\circ}$ C)	H_2 (bar)	t (min)	Benzyl alcohol yield (%)	Specific activity ($mol_{sub}/mol_{Pt} h$)
1	0.2Pt-SBA-15-500	1000	50	20	60	46.8	468
2	0.2Pt-SBA-15-500	1000	50	10	60	60.4	604
3	0.2Pt-SBA-15-500	500	50	10	60	78.2	391
4	0.2Pt-SBA-15-500-C	250	60	10	120	22.1	28
5	0.2Pt-SBA-15-500-C	250	50	20	120	12.9	16

Solvent: methanol (2 mL)

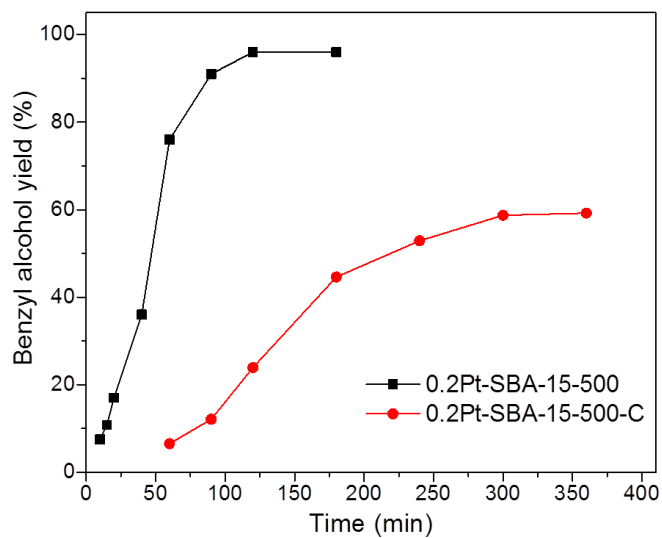


Fig. S9 Benzyl alcohol yield at different time using both 0.2Pt-SBA-15-500 and 0.2Pt-SBA-15-500-C catalysts. Reaction conditions: BZ/Pt = 500 for 0.2Pt-SBA-15-500 and 1:250 for 0.2Pt-SBA-15-500-C, solvent = methanol (2 mL), H₂ pressure = 10 bar, $T = 50\text{ }^{\circ}\text{C}$.

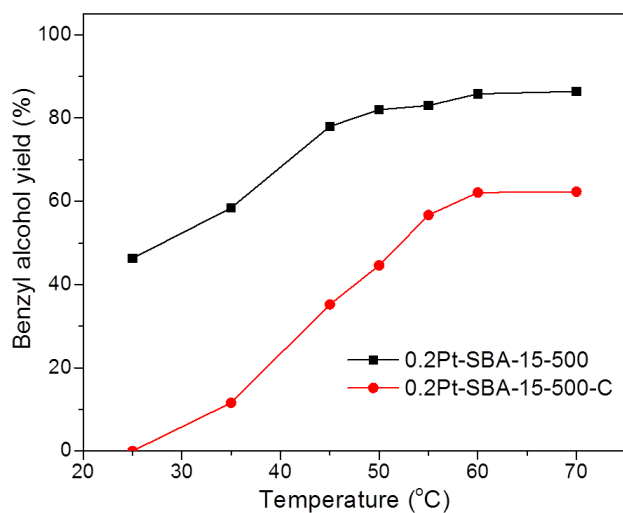


Fig. S10 Benzyl alcohol yield at different temperature using both 0.2Pt-SBA-15-500 and 0.2Pt-SBA-15-500-C catalysts. Reaction conditions: BZ/Pt = 500 for 0.2Pt-SBA-15-500 and 1:250 for 0.2Pt-SBA-15-500-C, solvent = methanol (2 mL), H₂ pressure = 10 bar, room temperature, $t = 1\text{ h}$ for 0.2Pt-SBA-15-500 and 3 h for 0.2Pt-SBA-15-500-C.

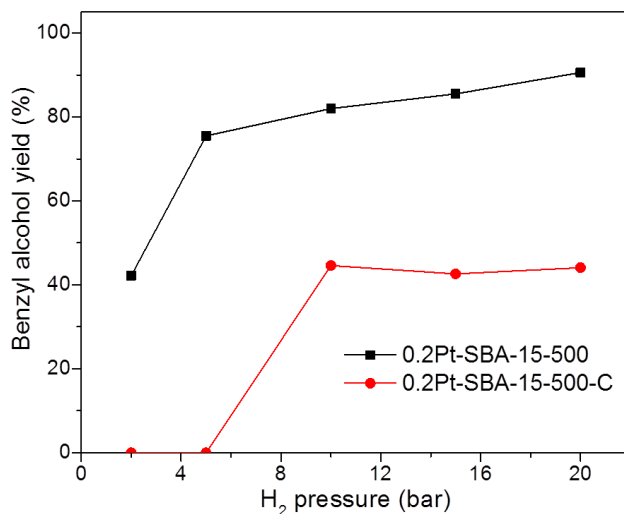


Fig. S11 Benzyl alcohol yield at different H₂ pressure using both 0.2Pt-SBA-15-500 and 0.2Pt-SBA-15-500-C catalysts. Reaction conditions: BZ/Pt = 500 for 0.2Pt-SBA-15-500 and 1:250 for 0.2Pt-SBA-15-500-C, solvent = methanol (2 mL), $T = 50\text{ }^{\circ}\text{C}$, $t = 1\text{ h}$ for 0.2Pt-SBA-15-500 and 3 h for 0.2Pt-SBA-15-500-C.

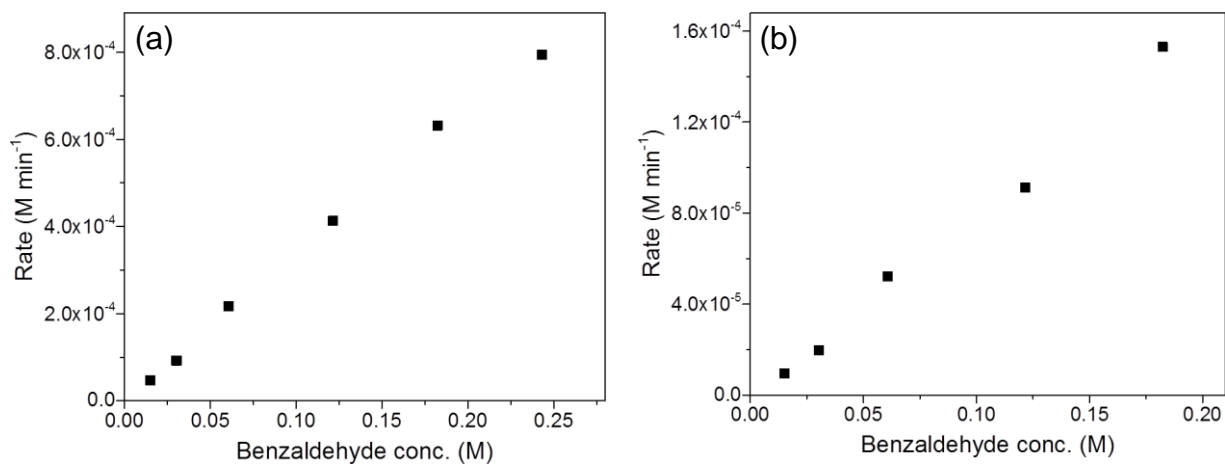


Fig. S12 Reaction rate vs. benzaldehyde concentration. Reaction conditions: catalyst = 12 mg (for 0.2Pt-SBA-15-500) and 24 mg (for 0.2Pt-SBA-15-500-C), solvent = methanol (2 mL), H₂ pressure = 10 bar, $t = 30\text{ min}$ (for 0.2Pt-SBA-15-500) and 3 h (for 0.2Pt-SBA-15-500-C), $T = \text{room temperature}$ (for 0.2Pt-SBA-15-500) and $35\text{ }^{\circ}\text{C}$ (for 0.2Pt-SBA-15-500-C).

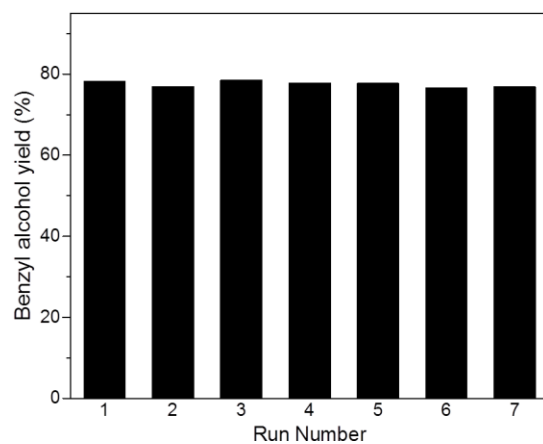


Fig. S13 Recycling test of 0.2Pt-SBA-15-500 catalyst for the hydrogenation of benzaldehyde. Reaction conditions: BZ/Pt = 500, solvent = methanol (2 mL), H₂ pressure = 10 bar, *T* = 50 °C, *t* = 1 h.

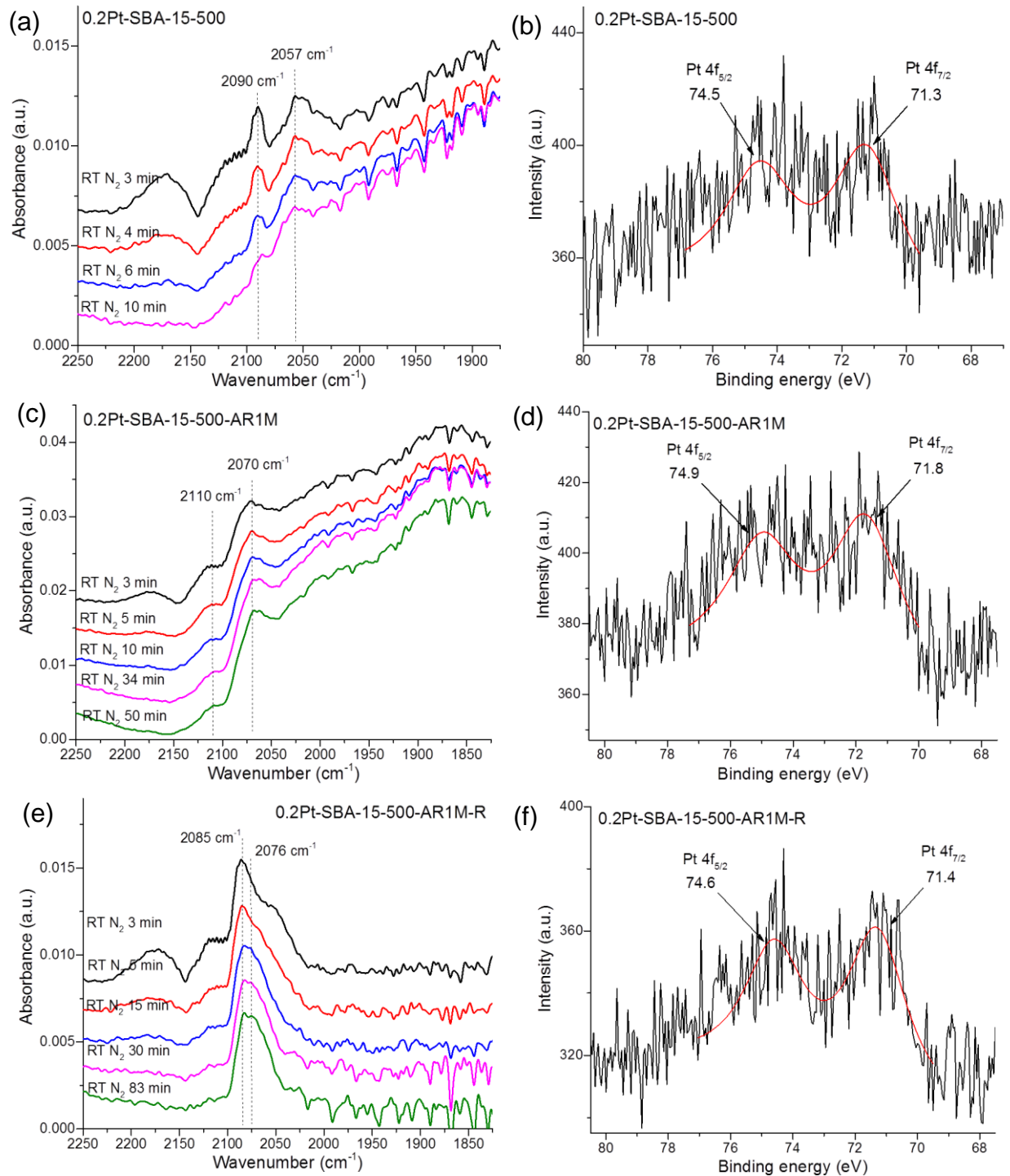


Fig. S14 IR spectra of CO adsorbed on different 0.2Pt-SBA-15-500 samples (a) before aqua regia treatment, (c) after aqua regia treatment, (e) after H₂ reduction of aqua regia treated sample, and their corresponding X-ray photoelectron spectra (b, d and f respectively).

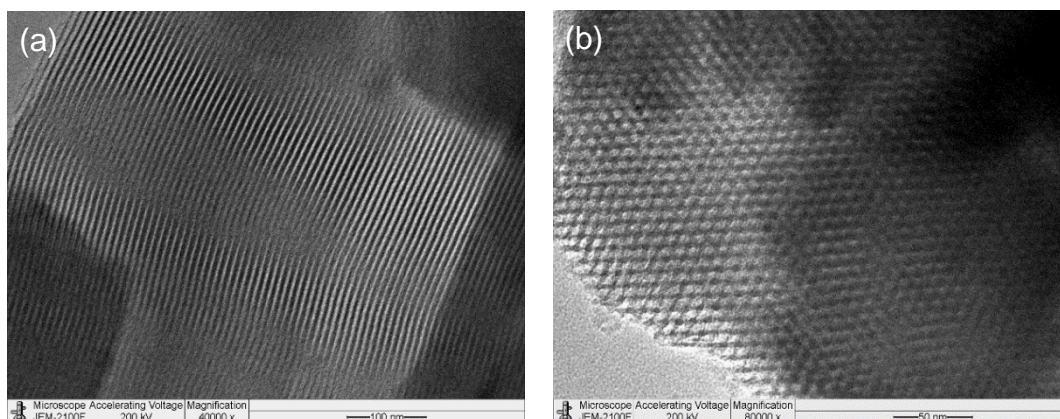


Fig. S15 TEM images of 0.2Pt-SBA-15-500 after the treatment with 1 M aqua regia.

Table S7 Hydrogenation of benzaldehyde (BZ) using 0.2Pt-SBA-15-500 catalysts before and after the treatment with aqua regia.

Entry	Catalyst	Treatment	Benzyl alcohol yield (%)	Specific activity (mol _{sub} /mol _{Pt} h)
1	0.2Pt-SBA-15-500	-	31.4	157
2	0.2Pt-SBA-15-500	1 M AR	13.8	69
3	0.2Pt-SBA-15-500	1 M AR / H ₂	25.2	126

Reaction conditions: BZ/Pt = 500, 2 mL methanol, 10 bar H₂, RT, 1 h.

Table S8 Hydrogenation of phenylacetylene (PhAc) using 0.2Pt-SBA-15-500 catalysts before and after the treatment with aqua regia.

Entry	Catalyst	Treatment	PhAc conversion (%)	Specific activity (mol _{sub} /mol _{Pt} h)	S _{styrene} (%)	S _{ethylbenzene} (%)
1	0.2Pt-SBA-15-500	-	11.2	3584	86.1	13.9
2	0.2Pt-SBA-15-500	1 M AR	7.8	2496	95.5	4.5
3	0.2Pt-SBA-15-500	1 M AR / H ₂	10.7	3424	94.2	5.8

Reaction conditions: PhAc/Pt = 8000, 2 mL methanol, 10 bar H₂, RT, 15 min.